KINETIC MEASUREMENTS DURING TRANSIENT FILM GROWTH ON ZINC

Yun Chen
Department of Engineering Physics, University of Wisconsin-Madison, Wisconsin 53706, USA
Rui F. M. Lobo
Institute of Materials and Surfaces Science and Engineering, Faculty of Science and Technology, New University of Lisbon, 2829-516 Caparica, Portugal
Diogo M. F. Santos and César A. C. Sequeira*
Institute of Materials and Surfaces Science and Engineering, Department of Chemical and Biological Engineering, Instituto Superior Técnico, Technical University of Lisbon, Av. Rovisco Pais, 1049-001 Lisboa, Portugal

The electrochemical behaviour of zinc has been extensively studied in alkaline and acid media, but only a few studies have been reported in neutral solutions, particularly in deaerated media. Zinc passivation in neutral medium and the effect of the ClO_4^- ion on the nucleation and growth of the passive layer is studied in this paper by a transient technique at different electrolyte concentrations and applied potentials. ZnO growth rate was shown to decrease with increasing electrolyte concentration. Moreover, passive layer growth occurred followed by pitting nucleation and growth. Film growth and pit nucleation are explained by means of the Macdonald and Engell-Stolica models.

Keywords: zinc; passivation; pitting.

INTRODUCTION

Zinc, one of the most widely used metals, cannot be worn in applications under applied stress due to its low creep resistance. It recrystallises rapidly after deformation at room temperature and, thus, cannot be work-hardened at room temperature. Creep resistance and recrystallisation temperature may be increased through alloying.[1] In the past decades, research on various aspects of corrosion of zinc has generated much technical information. Most of this wealth of information has been systematically and critically reviewed.[2]

The electrochemical properties of zinc are of most importance in its production and applications. For instance, electrowinning in zinc refining, electroplating in the production of zinc coatings, zinc batteries for energy storage, and zinc anodes for corrosion protection are all based essentially on zinc electrochemical properties. These properties include the relatively active position in the electromotive force series, fast and reversible dissolution/deposition kinetics, high overpotential for hydrogen evolution, and formation of passive film in slightly alkaline solutions.[2]

The electrochemical behaviour of zinc has been studied in alkaline media[3] due to the need of developing primary cells with high dissolution electrode activity and without passivation; it has also been studied in acid media[4] and slightly acid solutions[5] due to its applications in the Cl_2/Zn and Leclanché's batteries. Despite its extensive use in galvanised steels,[6] few studies have been reported in neutral solutions, particularly in deaerated media.[5, 7] In neutral solutions, with chemical agents that are not electrochemically reactive and that do not form insoluble salts or complex ions with zinc, the corrosion rate of zinc is not very different from that in distilled water. However, there are several species (*e.g.* certain anions) that greatly influence the corrosion processes of zinc in solutions. Láng and Horányi[8,9] demonstrated that the reduction of ClO_4^- ions takes place during the spontaneous dissolution of Zn in $HClO_4$. They furnished unambiguous evidence that such reduction leads to the formation of aggressive chloride ions

$$ClO_4^- + 4\ H_2O + 8\ e^- \rightarrow Cl^- + 8\ OH^- \qquad (1)$$

which play an important role in the passive layer formation as well as in the pitting process. In the absence of oxygen, the perchlorate ion adsorbs on the electrode surface and enhances the chemical dissolution of the interior ZnO layer to form Zn^{2+} (aq).[10,11] Moreover, its reduction promotes the formation of the less protective exterior passive layer as a result of the high amount of OH^- produced from reaction (1). The formation of a thicker less protective exterior layer and a thinner interior one in absence of O_2 is consistent with the nucleation and growth of pitting corrosion products.[12] The aggressiveness of the ClO_4^- ion towards the passivated Zn electrode in a neutral medium is studied in this paper by potentiostatic current-time transients at different electrolyte concentrations and applied potentials. Kinetic parameters were derived for passive layer growth, pit nucleation and its growth. The phenomenon of passivity, the electrochemistry of passivation, the models for pit initiation leading to passive film breakdown, and the kinetics of pit growth can be found in a number of sources.[13-15] In the present study, the nucleation rate increases with increasing electrolyte concentration and anodic applied potential. Film growth and pit nucleation are explained by means of the Macdonald and Engell-Stolica models.[16, 17]

EXPERIMENTAL

The working electrode was a disk made from a zinc rod (Aldrich, 99.999 %), with a geometric useful area of 0.243 cm^2, embedded in an epoxy resin. At the beginning of each electrochemical experiment, the electrode was polished with 800 grade emery paper under running water conditions and then thoroughly rinsed with purified water and dried with absorbent paper. A platinum sheet of 2 cm^2 geometric area was used as counter electrode and a saturated calomel electrode as reference, to which all potentials are referred. To avoid contamination with Cl^- ions, the reference electrode was connected to the working electrode through a bridge filled with the solution under test, the top of the bridge being pressed against the electrode surface to minimise

*e-mail: cesarsequeira@ist.utl.pt

the IR drop of the solution. The electrolyte solutions (0.001 - 0.1 M $KClO_4$ neutral solutions) were prepared from purified water (Milli-Q system) and $KClO_4$ (SIGMA, ACS Reagent, 99%). The solutions were deaerated with N_2 before each experiment, and during the experiments N_2 was passed over the non-stirred solutions. Tests for Cl^- ions in the ClO_4^- solutions revealed the absence of chloride ions after each experimental run.

The potentiostatic current-time transients were recorded by polarising potentiodynamically the working electrode from the starting potential of -1800 mV *vs.* SCE in the positive direction with the scan rate of 50 mVs^{-1} to a potential limit E_a ($\leq$ -500 mV *vs.* SCE) at which the current transients were recorded for 2 min. The selection of the -1800/-500 mV potential window was dictated by previous cyclic voltammetry measurements that showed an active/passive transition within that anodic span (Figure 1). A potentiostat/galvanostat (EG&G model 273) and a personal computer were used. Each experiment was performed with a freshly prepared solution and a newly polished set of electrodes. All measurements were carried out at room temperature (25 ± 0.5 ℃).

RESULTS AND DISCUSSION

Figure 1 shows a potentiodynamic current-potential curve for stationary zinc electrode in deaerated 0.1 M $KClO_4$ solution, at a scan rate of 1 mVs^{-1}. Its inspection reveals an active-passive transition prior to a certain critical breakdown potential, which is shown to be -700 mV *vs.* SCE. This value shifts to more anodic values when the potential is changed at higher scan rates, which explains why the potential window attained E_a values as high as -500 mV *vs.* SCE.

SEM observations (Figure 2) confirmed the different nature of the zinc surface, from its pretreated situation (A) to its anodic po-larisation showing passivity (B), starting of pit nucleation (C), and growth of pits (D).

The potentiostatic current-time transients for Zn in $KClO_4$ so-lutions with concentrations ranging from 0.001 to 0.1 M at various potential limits E_a (within the passive region) were recorded. Figure 3 represents some of these transients at E_a = -950 mV *vs.* SCE.

Figure 2. *SEM microphotographs of Zn surface. (A) pretreated Zn previous to its immersion in $KClO_4$; (B), (C), (D), Zn anodically polarised in 0.1 M $KClO_4$ at -800, -600, -400 mV vs. SCE, respectively, for 1 min*

Figure 1. *Typical potentiodynamic current-potential curve for stationary Zn electrode in deaerated 0.1 M $KClO_4$ at 25 ℃ and scan rate of 1 mV s^{-1}*
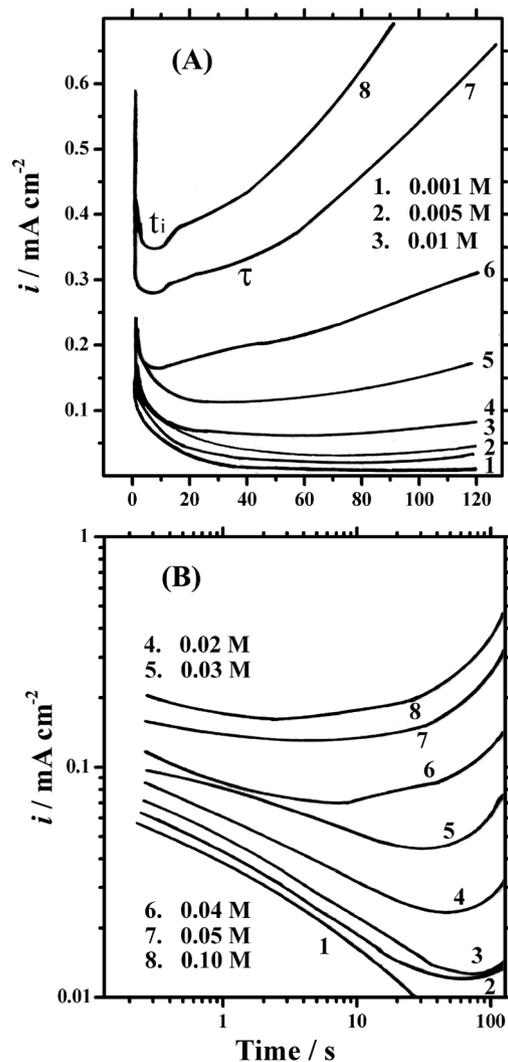
Figure 3. *Potentiostatic current-time transients for Zn in $KClO_4$ solutions with different concentrations at -950 mV (vs. SCE) and 25 ℃ in linear (A) and logarithmic (B) scales*

Inspection of the recorded results reveals that at low electrolyte concentration (≤ 0.01 M), the current decreases very rapidly with time to attain a steady state current value. The decrease in the transient current, i, is related to the growth of a ZnO layer on the electrode surface.[18-20] The film growth kinetics fits the model proposed by Macdonald *et al.*[16, 21] which is given by:

$$i = A\ t^{-n} \qquad (2)$$

where A and n are constants depending upon the potential limit E_a and the electrolyte concentration. The value of n represents the ZnO growth rate[22] and is given by the slope of the descending part of the log i – log t relationship (Figure 3B). The data given in Table 1 show that the values of n decrease with increasing electrolyte concentration [$KClO_4$]. This means that as the $KClO_4$ concentration increases, the growth rate of ZnO decreases. This aggressiveness of the ClO_4^- species, already discussed in the Introduction section, is well reported in the literature.[23-26] Favouring reaction (1), weakens the passive layer, which breaks and promotes pit initiation and growth. Considering that chemical analysis did not detect any traces of Cl^- after each experimental run, it can be assumed that reaction (1), although very aggressive towards the ZnO passive layer, is kinetically hindered. At concentrations higher than about 0.005 M, the current transient initially decreases to a minimum value i_m at a characteristic pitting time parameter t_i (incubation time). In other words, at low concentrations ($\sim$ 0.001 - 0.005 M) the passive layer grows very quickly and pitting corrosion is not induced. At moderate and higher concentrations passive layer growth occurs followed by a current increase that indicates pitting nucleation and growth.[27-29] The reciprocal of the incubation time (t_i^{-1}) is taken as the rate of pit nucleation. After t_i, the current transient exhibits two straight lines with two different slopes. The time at the inflection point is denoted as the induction time (τ). The first straight line may be considered to correspond to the period of pit nucleation, while the second line to that of pit growth.[30] The increase of current transient after t_i can be represented by the Engell-Stolica equation for pitting corrosion:[17]

$$i = B\ t^b \qquad (3)$$

where B and b are constants depending upon the applied potential and the concentration of $KClO_4$. The slopes of the log i - log t curves after t_i (b_1 for the first line and b_2 for the second line) as well as the pit nucleation rate (t_i^{-1}) and i_m for various $KClO_4$ concentrations are given in Table 1.

The values of b_1 are nearly constant, while those of b_2, t_i^{-1} and i_m increase with increasing perchlorate concentration. Moreover, current-time transient curves were recorded at various potential limits E_a for a given electrolyte concentration. Figure 4 represents

some transients on linear (a) and logarithmic (b) scales for Zn in 0.1 M $KClO_4$ solution at E_a potentials ranging from -1100 mV to -950 mV (*vs.* SCE).

For anodic potentials in the lower limits of the passive region, the rapid decrease of i to a steady value means that only the ZnO film is formed. For anodic potentials higher than about -1000 mV *vs.* SCE, ZnO growth as well as pit nucleation and growth occur. Table 2 lists the values of n, b_1, b_2, t_i^{-1} and i_m for the different anodic potentials
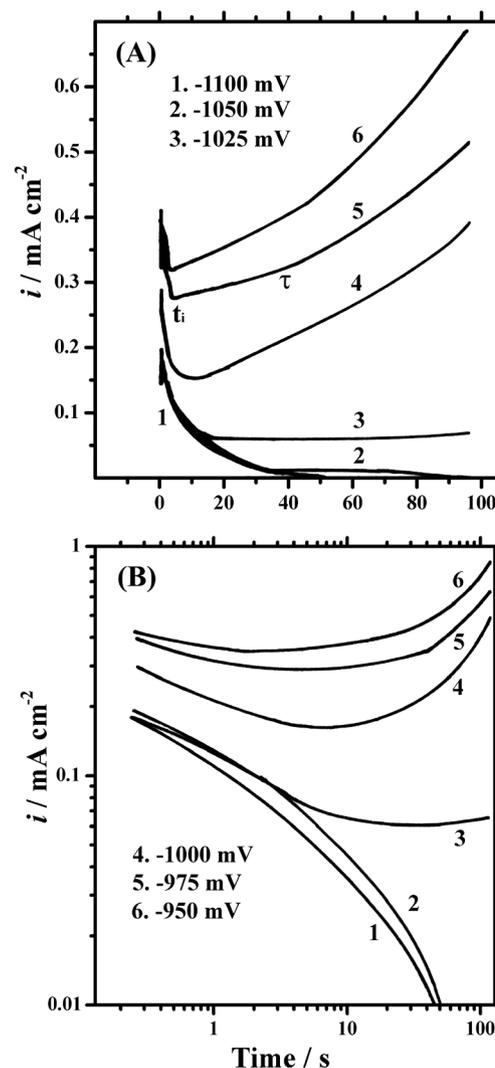
Figure 4. Potentiostatic current-time transients for Zn in 0.1 M $KClO_4$ solutions at different anodic potentials and 25 ºC in linear (A) and logarithmic (B) scales

Table 1. Effect of $KClO_4$ concentration on the transient behaviour of Zn in $KClO_4$ solutions at -950 mV *vs.* SCE for passive layer growth (n), pit nucleation (b_1, t_i^{-1} and i_m) and its growth (b_2)

[$KClO_4$] (M)	n	b_1	b_2	t_i^{-1} (s^{-1})	i_m (mAcm^{-2})
0.001	0.450	-	-	-	-
0.005	0.395	-	0.120	0.010	0.015
0.01	0.355	-	0.165	0.016	0.035
0.02	0.305	-	0.330	0.020	0.060
0.03	0.225	-	0.549	0.030	0.100
0.04	0.185	0.0991	0.575	0.138	0.160
0.05	0.150	0.0918	0.590	0.195	0.270
0.10	0.145	0.0998	0.625	0.251	0.336

Table 2. Effect of applied anodic potential on the transient behaviour of Zn in 0.1 M $KClO_4$ solutions at 25 ºC for passive layer growth (n), pit nucleation (b_1, t_i^{-1} and i_m) and its growth (b_2)

E_a (mV)	n	b_1	b_2	t_i^{-1} (s^{-1})	i_m (mA cm^{-2})
-1100	0.450	-	-	-	-
-1050	0.355	-	-	-	-
-1025	0.320	-	0.050	0.045	0.060
-1000	0.285	-	0.475	0.115	0.150
-975	0.235	0.0942	0.515	0.225	0.230
-950	0.145	0.0998	0.625	0.251	0.336

used to obtain the results given in Figure 4. The values of n decrease with increasing applied potential, the values of b_1 are nearly constant, while those of b_2, t_i^{-1} and i_m enhance with the potential limit E_a.

CONCLUSIONS

The corrosion behaviour of Zn in $KClO_4$ solutions was studied by current-time transient measurements. Previous potentiodynamic curves exhibited active/passive transitions. Zinc passivation is due to the formation of a ZnO layer on the electrode surface. Higher concentrations of ClO_4^- ions (>0.005 M) break down the passive layer and cause pitting corrosion at a certain anodic potential. The rate of pit nucleation increases with increasing both ClO_4^- concentration and applied anodic potential.

ACKNOWLEDGEMENTS

REFERENCES

1. Morgan, S. W. K.; *Zinc and its Alloys and Compounds*, Wiley: New York, 1985.
2. Zhang, X. G.; *Corrosion and Electrochemistry of Zinc*, Plenum: New York, 1996.
3. McKrube, M. C. H.; Macdonald, D. D.; *J. Electrochem. Soc.* **1981**, *128*, 524.
4. Kim, J. T.; Jorné, J.; *J. Electrochem. Soc.* **1980**, *127*, 7.
5. Baugh, L. M.; *Electrochim. Acta* **1979**, *24*, 657.
6. Deslouis, C.; Duprat, M.; Tulet-Tournillon, C.; *Corros. Sci.* **1989**, *29*, 13.
7. Hamnett, H.; Mortimer, R. J.; *J. Electroanal. Chem.* **1987**, *234*, 185.
8. Láng, G.; Inzelt, G.; Vrabecz, A.; Horányi, G.; *J. Electroanal. Chem.* **2005**, *582*, 249.
9. Láng, G.; Horányi, G.; *J. Electroanal. Chem.* **2003**, *552*, 197.
10. Sziráki, L.; Szöcs, E.; Philbáth, Zs.; Papp, K.; Kálmán, E.; *Electrochim. Acta* **2001**, *46*, 3743.
11. Justo, M. J.; Ferreira, M. G. S.; *Corros. Sci.* **1993**, *34*, 533.
12. Szklarska-Smialowska, Z.; *Pitting Corrosion of Metals*, NACE: Houston, 1986.
13. Sato, N.; Hashimoto, K., eds.; *Passivity of Metals and Semiconductors*, Pergamon: Oxford, 1990, part 1.
14. Kaesche, H.; *Die Korrosion der Metalle*, 3rd ed., Springer-Verlag: Berlin, 1990.
15. Frankel, G. S.; Scully, J. R.; Jahnes, C. V.; *J. Electrochem. Soc.* **1996**, *143*, 1834.
16. Macdonald, D. D.; Urquidi-Macdonald, M.; *J. Electrochem. Soc.* **1990**, *137*, 2395.
17. Engell, H. J.; Stolica, D. N.; *Z. Phys. Chem. Unterr.* **1959**, *20*, 113.
18. Sziráki, L.; Cziráki, A.; Geröcs, I.; Vértesy, Z.; Kiss, L.; *Electrochim. Acta* **1998**, *43*, 175.
19. Triboulet, R.; Perrière, J.; *Prog. Crystal Growth Char. Mat.* **2003**, *47*, 65.
20. Chen, X. L.; Geng, X. H.; Xue, J. M.; Li, L. N.; *J. Crystal Growth* **2007**, *299*, 77.
21. Chao, C. Y., Lin, L. F.; Macdonald, D. D.; *J. Electrochem. Soc.* **1981**, *128*, 1187.
22. Kim, J.; Pyun, S.; *Electrochim. Acta* **1995**, *40*, 1863.
23. Ujvári, M.; Láng, G.; Horányi, G.; *J. Appl. Electrochem.* **2002**, *32*, 581.
24. Cachet, C.; Wiart, R.; *J. Electroanal. Chem.* **1981**, *129*, 103.
25. Cachet, C.; Ganne, F.; Maurin, G.; Petitjean, J.; Vivier, V.; Wiart, R.; *Electrochim. Acta* **2001**, *47*, 509.
26. Cachet, C.; Ganne, F.; Joiret, S.; Maurin, G.; Petitjean, J.; Vivier, V.; Wiart, R.; *Electrochim. Acta* **2002**, *47*, 3409.
27. Amin, M. A.; *Electrochim. Acta* **2005**, *50*, 1265.
28. Abd El Aal, E. E.; *Corros. Sci.* **2002**, *44*, 2041.
29. Assaf, F. H.; Abd El-Rehiem, S. S.; Zaky, A. M.; *Mat. Chem. Phys.* **1999**, *58*, 58.
30. Milosev, I.; Metikos-Hukovic, M.; *J. Electrochem. Soc.* **1991**, *138*, 61.